

Air–Hydrogen Heat Exchangers for Advanced Space Launchers

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This paper deals with air–hydrogen heat exchangers intended to provide in-flight oxygen collection capability to a reusable or semireusable two-stages-to-orbit launcher with an oxygen collection phase in supersonic cruise at Mach 2.5. It aims to present a theoretical but mainly technological and experimental feasibility study of heat exchangers sufficiently efficient and reliable to suit the extreme requirements of this application. Two precoolers of two different types (shell and tubes, and plate and fins) have been selected and designed with the objective of fulfilling all constraints of the concept in terms of performance, leak tightness, reliability, compactness, etc. This design process has been validated with four subscaled breadboards (two of each type) tested on two test benches (for performance and leak tightness), developed by Belgium and Spain, in on-design and off-design conditions. All these results highlight the suitability of the new technologies given the extreme requirements of the concept. An optimum design for each technology is recommended considering its proper advantages and disadvantages. An innovative precooler technology is presented and tested.

Nomenclature

A	=	surface, m ²
A_{sf}	=	fin cross section, m ²
AU	=	global heat transfer coefficient, W/K
C	=	fluid velocity, m/s
\dot{C}	=	capacitive flow rate, $Q \cdot c_p$, W/K
Cr	=	capacitive flow rate, $(Q \cdot c_p)_{\min}/(Q \cdot c_p)_{\max}$
Cv	=	flow coefficient of a valve
c_p	=	specific heat at constant pressure, J/kg · K
D_{curv}	=	diameter of curvature, m
D_{hyd}	=	hydraulic diameter, m
Di	=	inside diameter, m
D_p	=	depth, m
d	=	outside diameter, m
e	=	thickness, m
f	=	friction factor
h	=	convective heat transfer coefficient, W/m ² K
h_f	=	fin height, m
K	=	charge loss coefficient
Kc	=	contraction coefficient
Ke	=	expansion coefficient
k	=	conductivity, W/mK
L_p	=	passage length, m
l	=	length of tube, m
Nu	=	Nusselt number
n	=	number of passes

P	=	pressure, Pa
P_f	=	perimeter of a fin, m
Pr	=	Prandtl number
Q	=	mass flow rate, kg/s
Re	=	Reynolds number
R_{th}	=	thermal resistance, K/W
T	=	temperature, K
U	=	global heat transfer coefficient, W/Km ²
xd	=	diagonal pitch coefficient
xl	=	longitudinal pitch coefficient
xt	=	transversal pitch coefficient
ΔP	=	pressure drop, Pa
ε	=	effectiveness, %
ρ	=	density, kg/m ³
σ	=	ratio of the finned surface and the total transfer surface
ϕ	=	contraction ratio

Subscripts

acc	=	acceleration part
atm	=	atmospheric
c	=	cold side
D	=	diameter
f	=	fin
$f, 0$	=	finned surface
h	=	hot side
i	=	inlet
max	=	maximum
min	=	minimum
o	=	outlet
p	=	pass

I. Introduction

IN MOST of the past and current space launchers, a large and unused quantity of energy is generally stored in the liquid hydrogen present onboard as a fuel. In the 1950s, a first application was proposed to recover a part of this energy with the liquefied air cycle

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